

Novel Fission-Product Separation Based on Room Temperature Ionic Liquids

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Research Objectives

The overall goal of this project is to develop a new ionic liquid based solvent extraction process for separation of Cs-137 and Sr-90 from tank wastes.

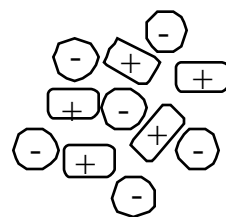
- **To synthesize new ionic liquids tailored for the extractive separation of Cs^+ and Sr^{2+} .**
- **To select optimum macrocyclic extractants through studies of complexation of fission products with macrocyclic extractants and transport in new extraction systems based on ionic liquids.**
- **To develop efficient processes to recycle ionic liquids and crown ethers via electrochemistry.**
- **To investigate chemical stabilities of ionic liquids under strong acid, strong base, and high level radiation conditions.**


Why Ionic Liquids?


Ionic systems consisting of salts that are liquid at ambient temperatures can act as solvents for a broad spectrum of chemical species.

- ***Nonvolatility***
- ***Ionicity***
- ***Tunable Hydrophobicity***
- ***Tunable Lewis Acidity***
- ***Large Electrochemical windows***
- ***Thermal Stability***
- ***Nonflammability***
- ***Wide Liquid-Phase Temperature.***
(-100°C to around 300°C)

Ionic Liquid




 = Anion

 = Cation

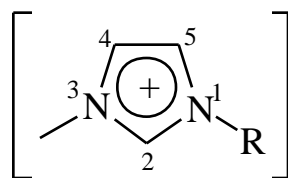
Organic Solvent



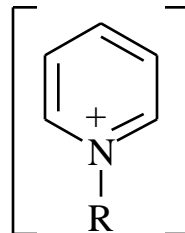
 = Neutral
Molecule

Range of Organic Cations and Anions Typically Used to Prepare Room-Temperature Ionic Liquids

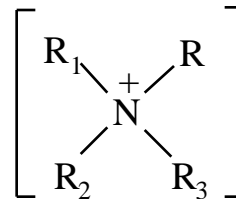
Most commonly used cations:



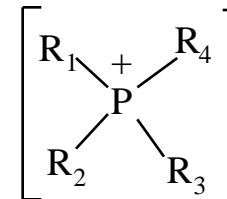
1-alkyl-3-methyl-imidazolium



N-alkyl-pyridinium



Tetraalkyl-ammonium



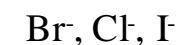
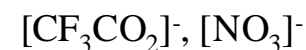
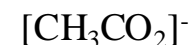
Tetraalkyl-phosphonium
($R_{1,2,3,4}$ = alkyl)

Some possible anions:

water-insoluble



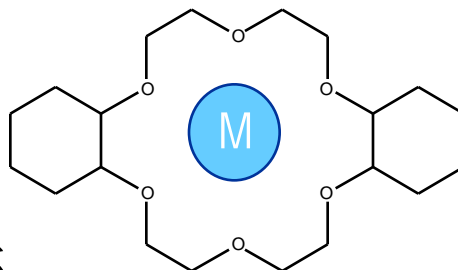
water-soluble



Most commonly used alkyl chains:

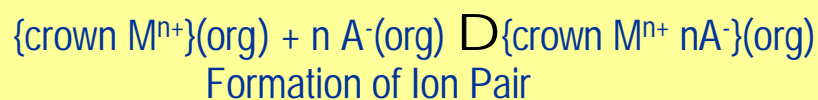
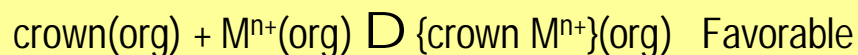
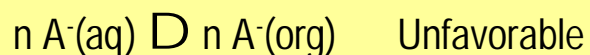
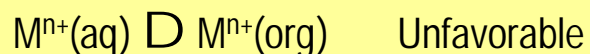
ethyl octyl
butyl decyl
hexyl

Comparison of Solvent Extractions Based on Molecular Solvents and Ionic Liquids

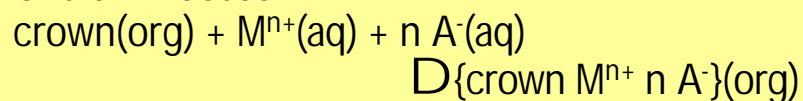


Molecular Solvents

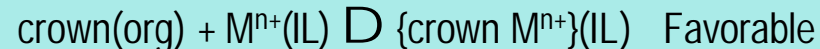
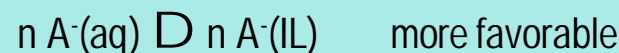
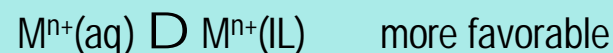
Ionic Liquids (IL)



Overall Process:

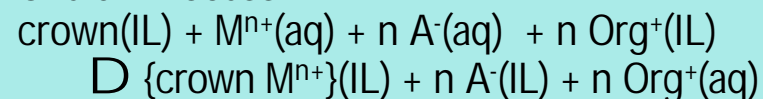


Thermodynamically Unfavorable



Ion Exchange – Dietz & Rogers

Overall Process:



Thermodynamically favorable

Summary of Completed Research

- **Development of Highly Selective Extraction Process for Cs⁺ Based on Calixarenes**
- **Demonstration of Facilitated Sacrificial Ion-Exchange Extraction Processes to Reduce the Loss of ILs and to Increase Extractive Strength of ILs**
- **Development of Recyclable IL-Based Extraction Systems**
- **Optimization of Selectivities of Extractants via Systematic Change of ILs**
- **Development of an Electrochemical Method for Recycling the Ionic Liquid-ionophore Extractant Phase Following the Extraction of Cs⁺ and Sr²⁺**
- **Synthesis of New Ethylene-Glycol Functionalized Bis-Imidazolium Ionic Liquids and Sr²⁺/Cs⁺ Partitioning Studies**

Anal. Chem. 2004, 76, 2773-2779.
Anal. Chem. 2004, 76, 3078-3083.

Comparison of Sr-Extraction Results Obtained Using Ionic Liquids and Conventional Solvents.

<i>Extract Phase</i>	<i>K_d^a With 0.15 M crown ether^a</i>	<i>K_d Without crown ether</i>
<i>BuMe₂ImPF₆</i>	4.2	0.67
<i>BuMeImPF₆</i>	2.4×10	0.89
<i>EtMe₂ImTf₂N</i>	4.5×10^3	0.81
<i>EtMeImTf₂N</i>	1.1×10^4	0.64
<i>PrMe₂ImTf₂N</i>	1.8×10^3	0.47
<i>PrMeImTf₂N</i>	5.4×10^3	0.35
<i>C₆H₅CH₃</i>	7.6×10^{-1}	nm ^a
<i>CHCl₃</i>	7.7×10^{-1}	nm

Messages:

- Key Role Played By Crown Ether
- Ion-Exchange Effect

14,000
Enhancement

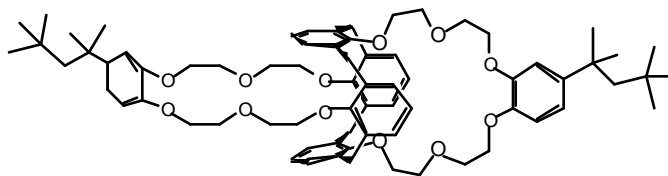
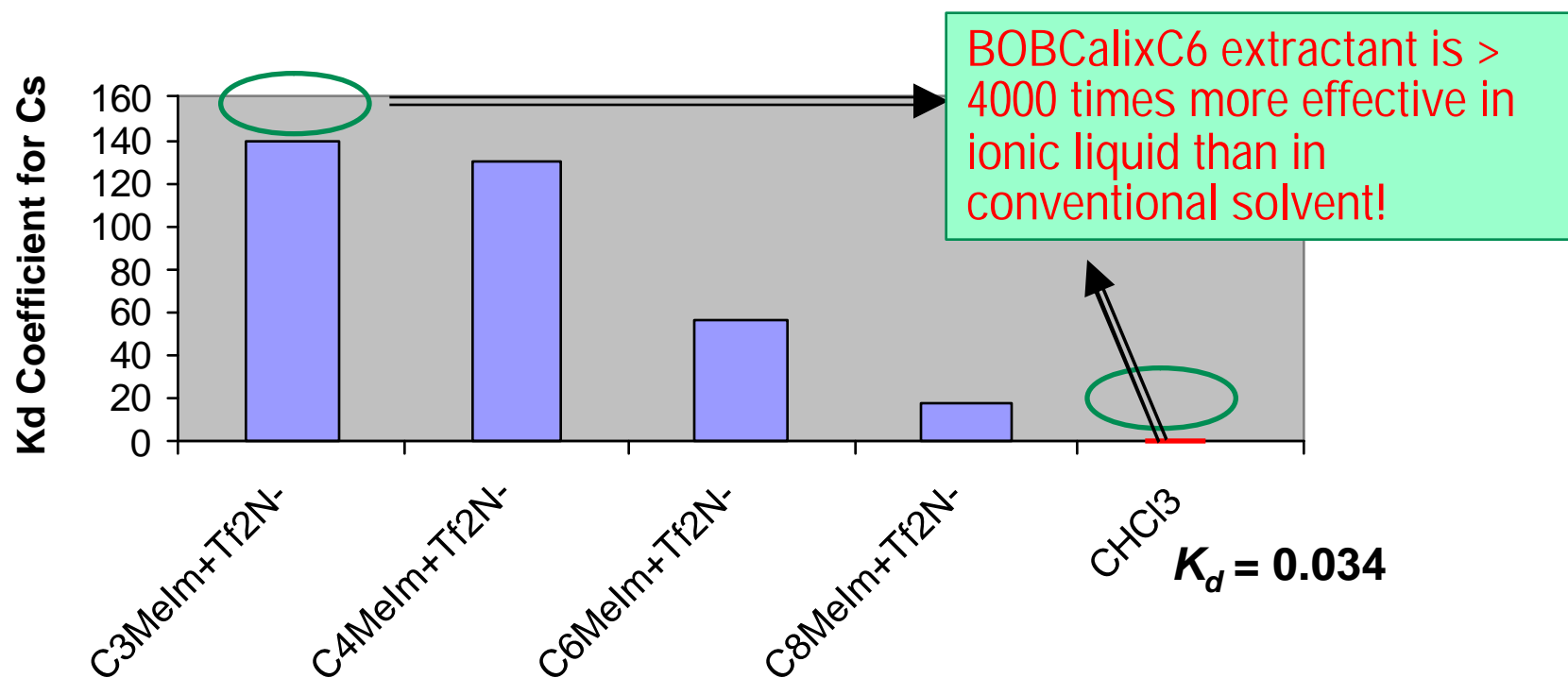
^a The crown ether used in this experiment is dicyclohexane-18-crown-6.

^b nm : not measurable.

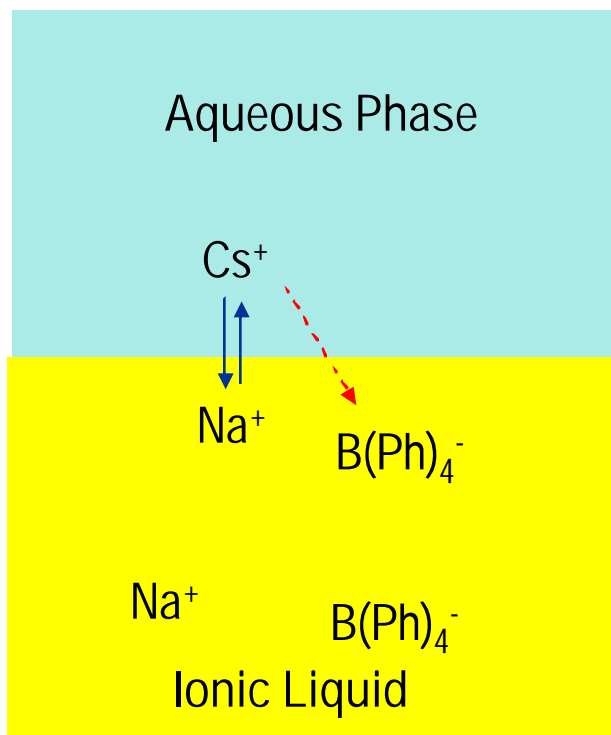
S. Dai, Y. H. Ju, and C. E. Barnes "Solvent extraction of strontium nitrate by a crown ether using room-temperature ionic liquids" J. Chem. Soc. Dalton Trans. 1999, 1201-1202.

S. Dai, Y. H. Ju, and H. Luo, "Separation of Fission Products Based on Ionic Liquids" in International George Papatheodorou Symposium, Patras Science Park, 1999, p254-262

Very High Capture of Cesium Measured for Ionic Liquid-Based Solvents Containing BOBCalixC6



Separation Systems Based on Facilitated Ion-Exchange Recognition



Facilitated Transport via Ion-Exchange Recognition

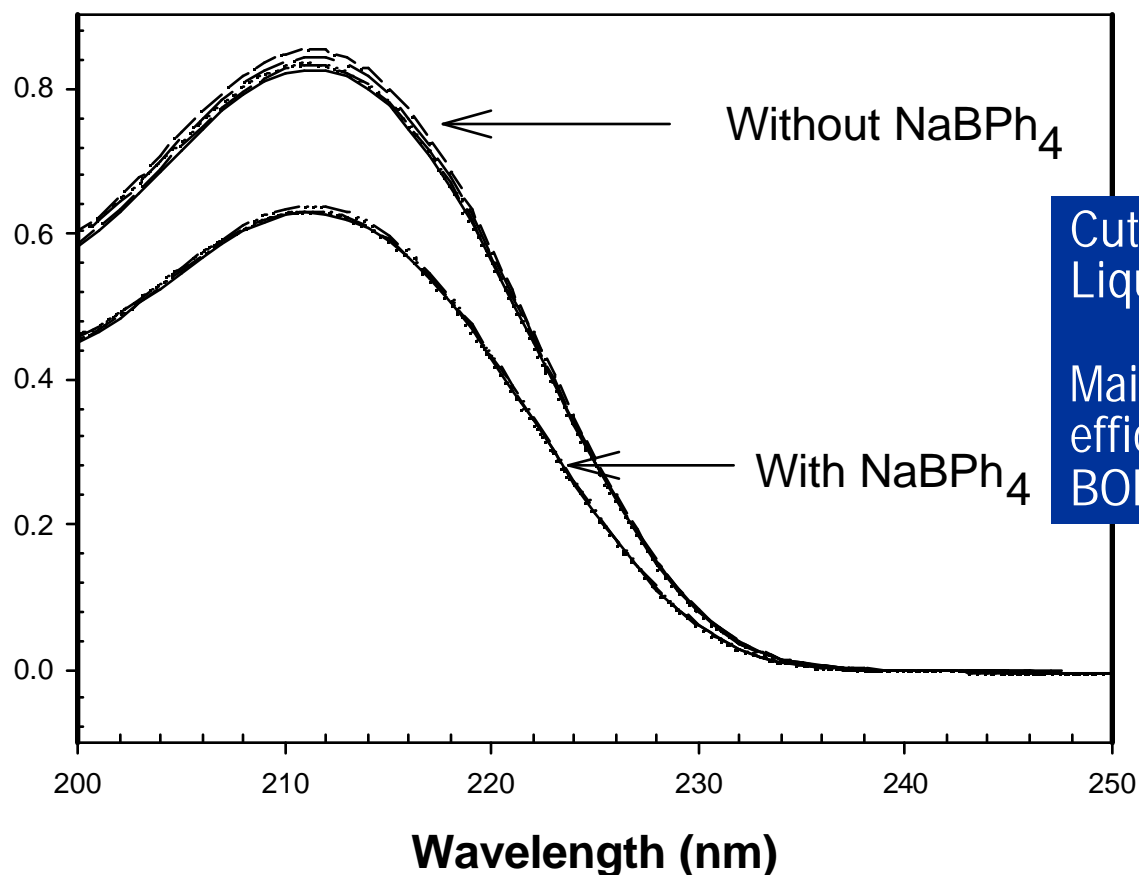
Liquid Membranes Containing NaB(Ph)_4 or $\text{NaB(Ph-F}_4)_4$ in Ionic Liquids

NaB(ph)_4	$K_d (\text{Cs})$	Initial CsCl Concentration
$7.69 \times 10^{-3} \text{ M}$	0.21	88 ppm
$2.34 \times 10^{-3} \text{ M}$	0.32	320 ppm

$\text{NaB(ph-F}_4)_4$	$K_d (\text{Cs})$	Initial CsCl Concentration
$1.85 \times 10^{-2} \text{ M}$	0.65	88 ppm
$5.87 \times 10^{-2} \text{ M}$	0.71	88 ppm

Na^+
Sacrificial Ion Exchanger

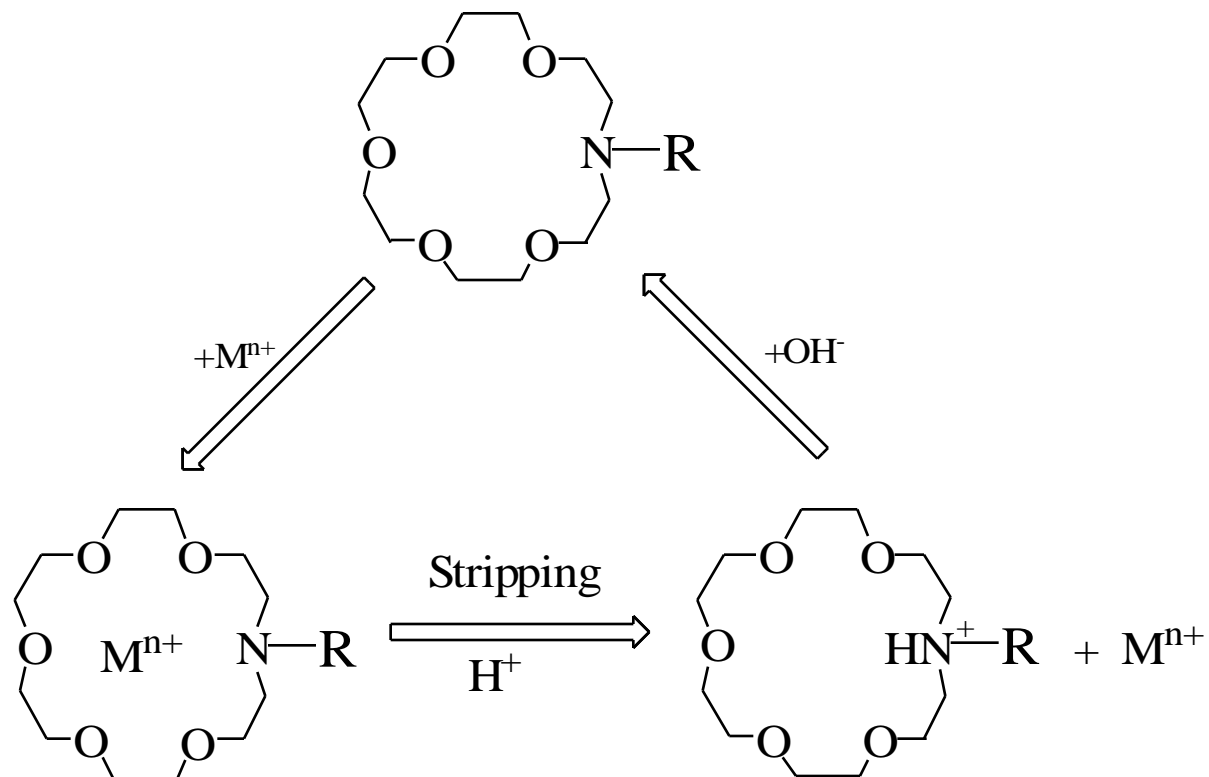
UV-Visible Spectra of Ionic Liquids Lost to Aqueous Solutions During Extraction with and Without NaBPh₄



Cut Loss of Ionic Liquid by 20%

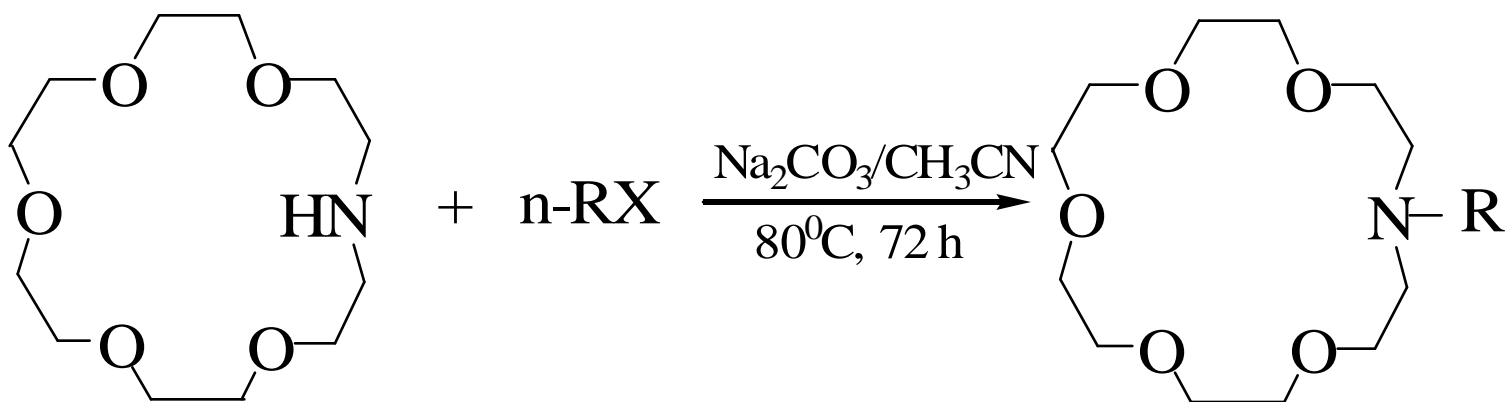
Maintain extraction efficiencies for BOBCalixC6

Development of Stripping Protocol to Recycle Macrocyclic Extractants



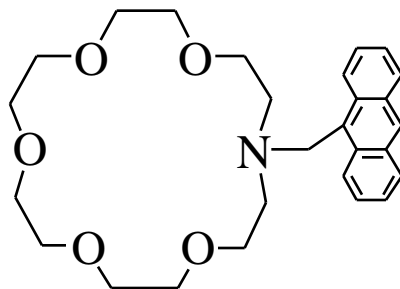
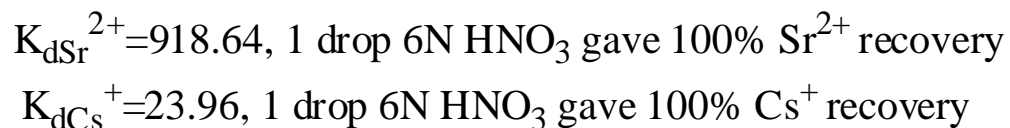
Luo, H.; Dai, S.; Bonnesen, P. V. *Anal. Chem.* 2004, in press

Synthesis of 1-Aza-18-crown-6 Derivatives



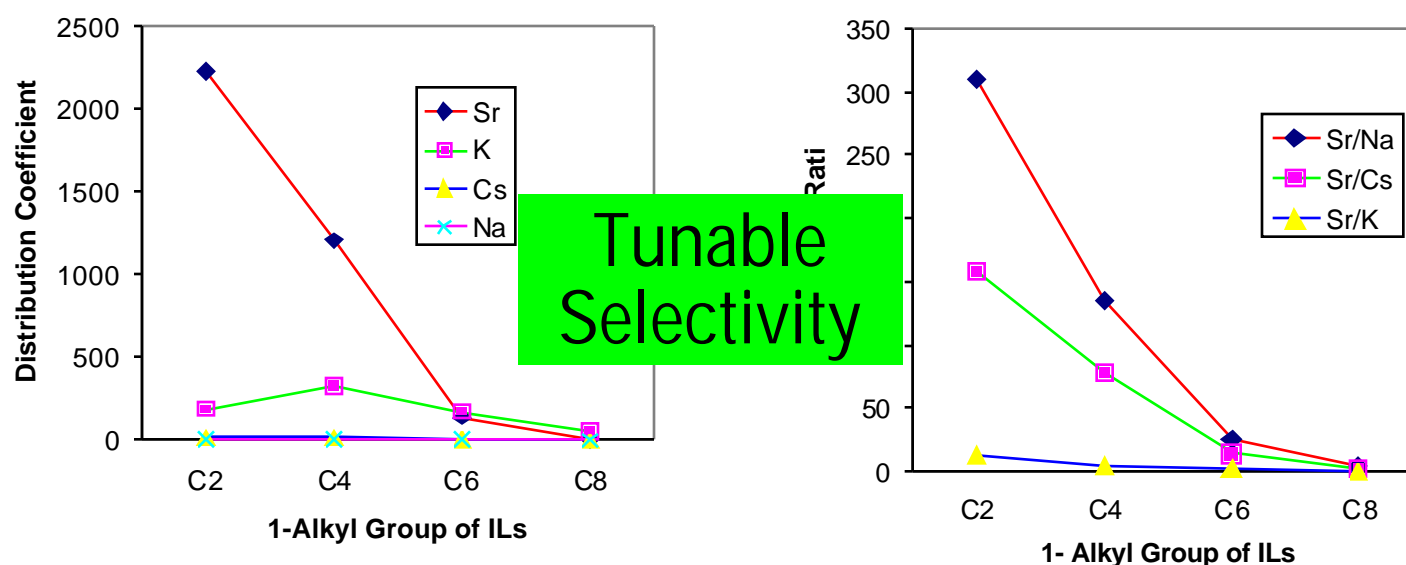
1. R = ethyl, X = Br
2. R = n-butyl, X = Br
3. R = n-hexyl, X = Br
4. R = n-octyl, X = Br

5. R = n-dodecyl, X = Br
6. R = n-hexadecyl, X = Br
7. R = $\text{CF}_3(\text{CF}_2)_5\text{CH}_2\text{CH}_2-$, X = I
8. R = 9-anthracenylmethyl, X = Cl



$K_{dSr}^{2+}=3.77$, 1 drop 6N HNO_3 gave 95% Sr^{2+} recovery
 $K_{dCs}^{+}=14.9$, 1 drop 6N HNO_3 gave 100% Cs^{+} recovery

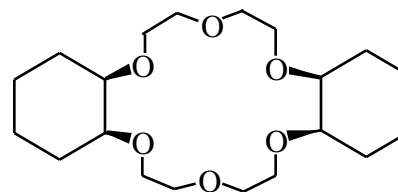
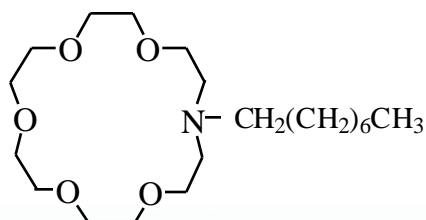
Effect of 1-Alkyl Group of ILs on Efficiency and Selectivity of Competitive Sr, K, Na, Cs Cation Extraction from Aqueous Solutions into ILs Containing 1-Octyl-aza-18-crown-6



- For C₂mim-Tf₂N & C₄mim-Tf₂N, the extraction efficiency is Sr²⁺ >> K⁺ > Cs⁺ > Na⁺.
- In C₆mim-Tf₂N & C₈mim-Tf₂N, the order is K⁺ > Sr²⁺ > Cs⁺ > Na⁺.

Comparison of Extraction Results of 1-Octyl-aza-18-crown-6 with DCH18C6

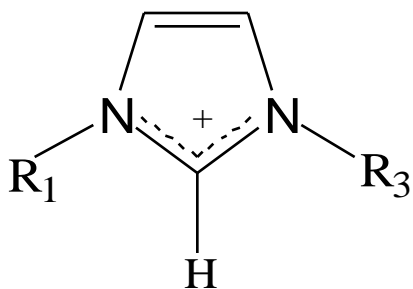
OAZ18C6	DCH18C6
Recyclable	Non-recyclable
Non-commercial available	Commercial available
$D_{\text{Sr}}: 8426 \text{ (in } C_2) \text{ and } 1072 \text{ (in } C_4)$ $D_{\text{Cs}}: 25.21 \text{ (in } C_2) \text{ and } 25.73 \text{ (in } C_4)$	$D_{\text{Sr}}: 10734 \text{ (in } C_2) \text{ and } 935 \text{ (in } C_4)$ $D_{\text{Cs}}: 589 \text{ (in } C_2) \text{ and } 380 \text{ (in } C_4)$
Extraction Selectivity: $\text{Sr}^{2+} > \text{K}^+ > \text{Cs}^+ > \text{Na}^+$	Extraction Selectivity: $\text{K}^+ > \text{Sr}^{2+} > \text{Cs}^+ > \text{Na}^+$



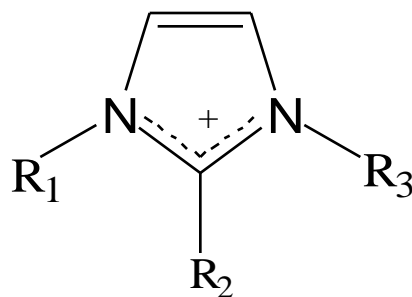
Future Research Plans

1. Synthesis and Optimization of ILs Tailored for Solvent Extraction of Fission Products
2. Synthesis and Study of Recyclable Crown Ethers
3. Optimization of Anions of ILs for Extraction of Fission Products
4. Sacrificial Ion-Exchange Method for Synergistic Extraction of Metal Ions and Reduction of ILs Loss
5. Development of an Electrochemical Method for the Non-Destructive Removal of Extracted Cs^+ and Sr^{2+}
6. Study of Stabilities of ILs in Harsh Chemical and Radiation Environments

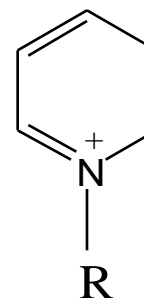
Synthesis and Optimization of Ionic Liquids Tailored for Solvent Extraction of Fission Products



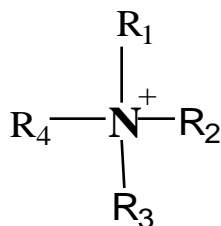
1,3-Dialkylimidazolium-Based



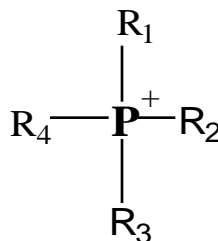
C(2)-Position Substituted
Imidazolium-Based



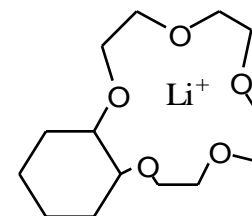
Pyridinium-Based



Quaternary Ammonium-Based

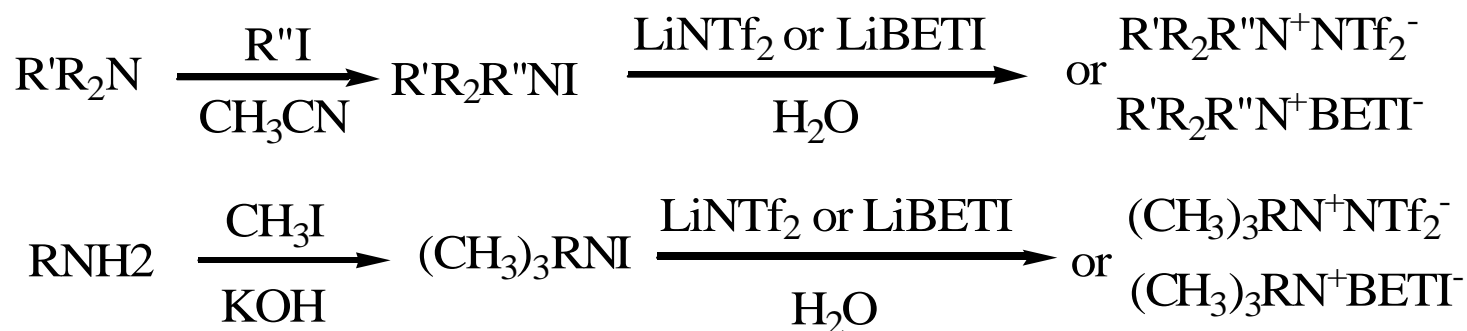
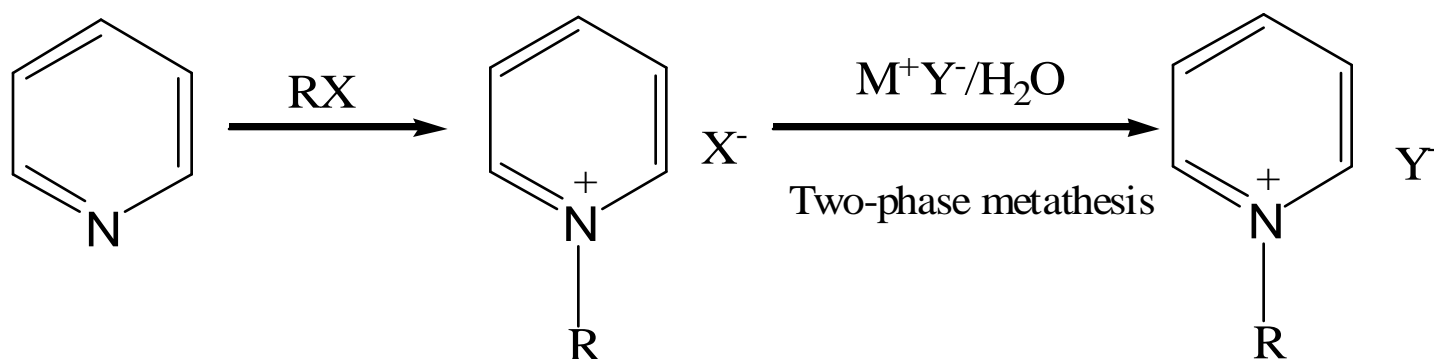


Tetraalkylphosphonium-Based

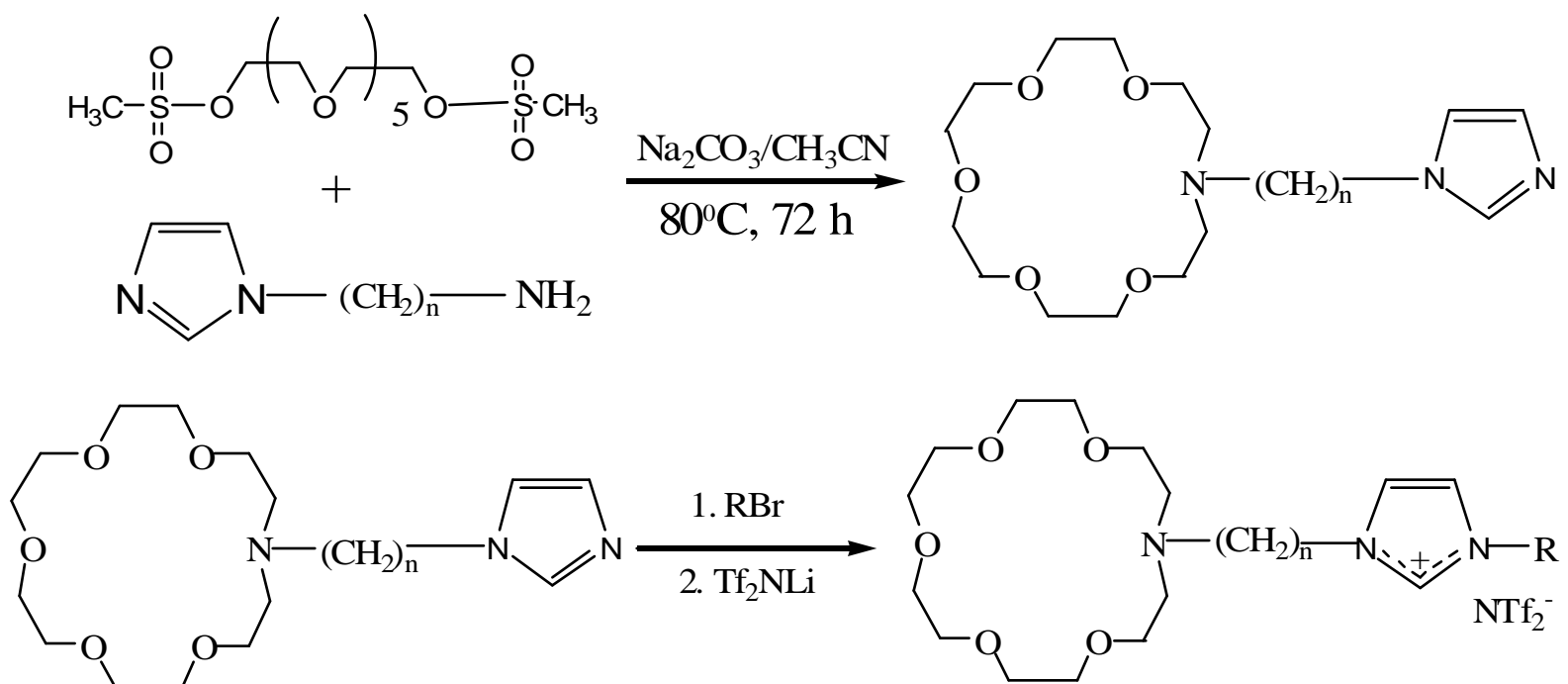


Metal Complexes-Based

Typical Synthesis of Ionic Liquids Based on Alkylpyridinium and Quaternary Ammonium

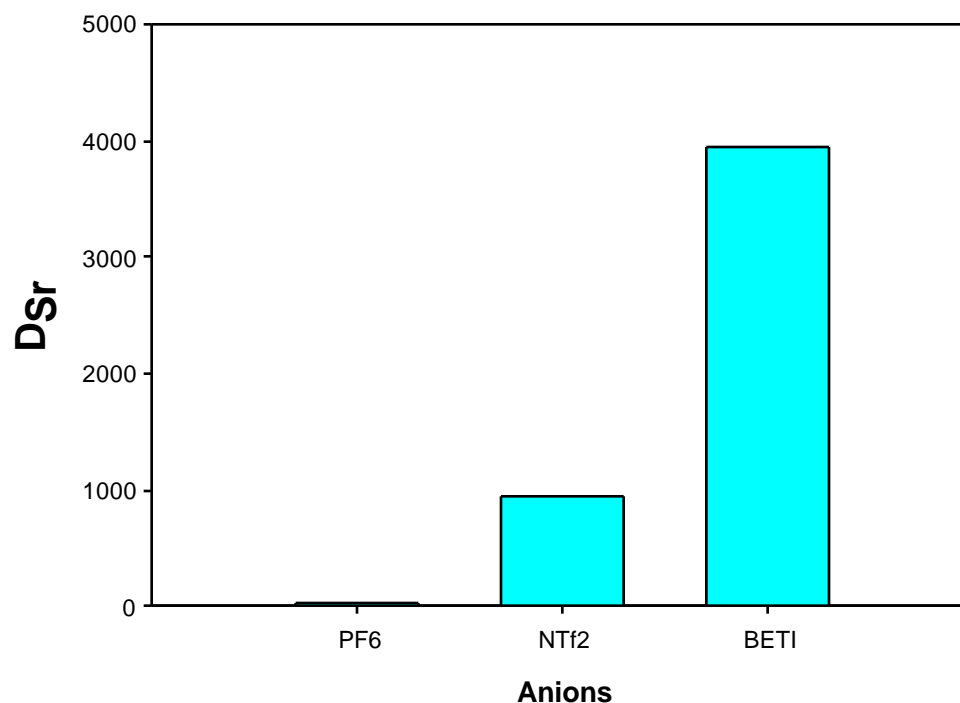


Synthesis of Task-Specific Ionic Liquids Containing an Aza crown Ether Fragment



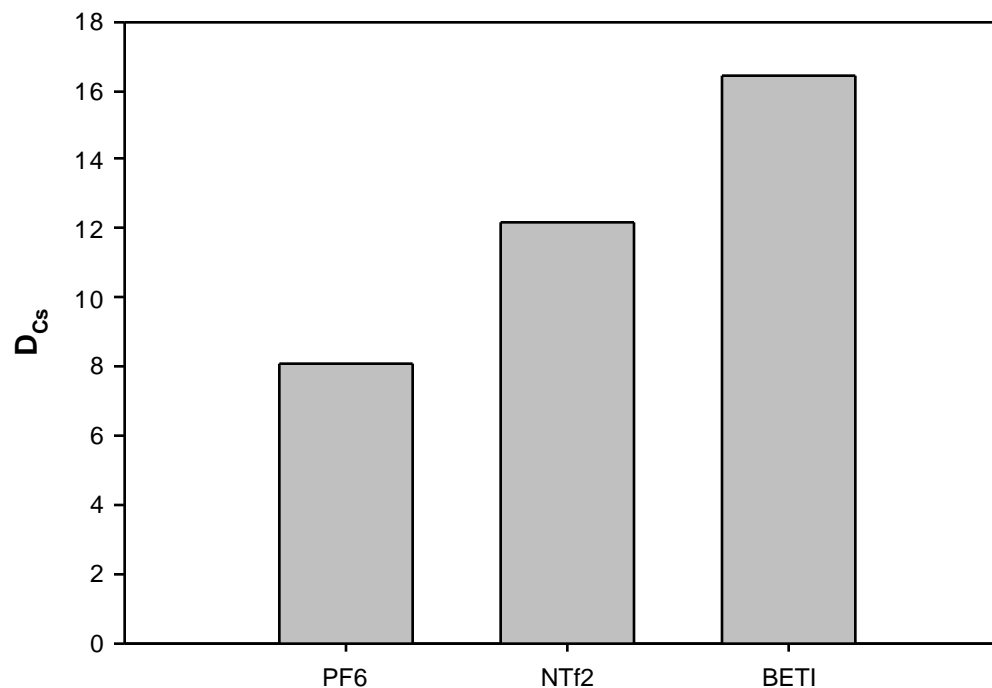
Dependence of D_{sr} on IL Anions of $[C_4mim]$ -based ILs Containing DCH18C6.

- D_{sr} value increases dramatically as the anion changed from PF_6^- to NTf_2^- to $BETf^-$. D_{sr} for $BETf^-$ is more than 200 times larger than that for PF_6^- .
- The increase of D_{sr} with the hydrophobicity of the counter anions is in sharp contrast to the observation with the cation effect of ILs. In the latter case, D_{sr} decreases with the hydrophobicity of the IL cations.



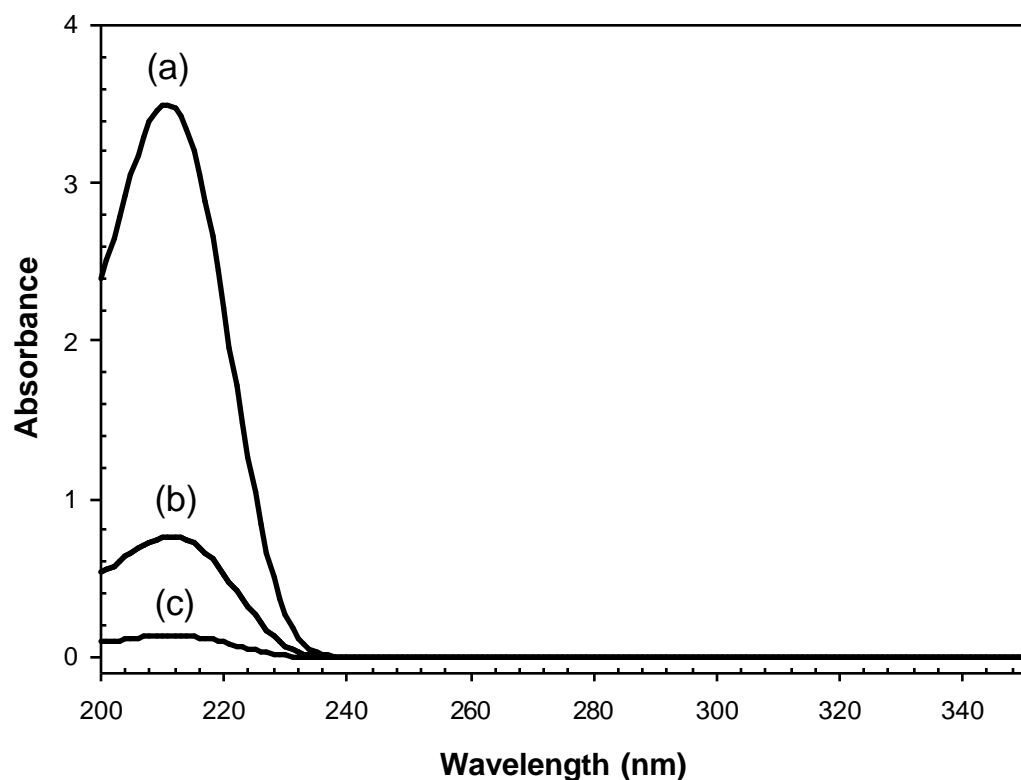
Anion Effect on D_{Cs} of $[C_4mim][X]$ Containing BOBCalixC6

- D_{Cs} values increase slightly as the anion changed from PF_6 to NTf_2 to $BETf$.

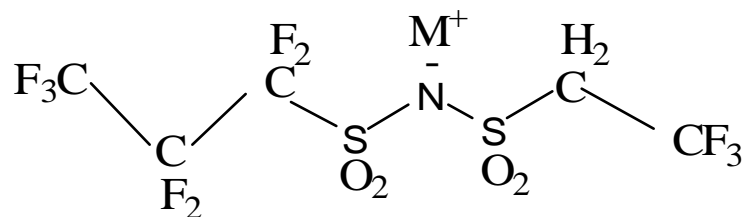
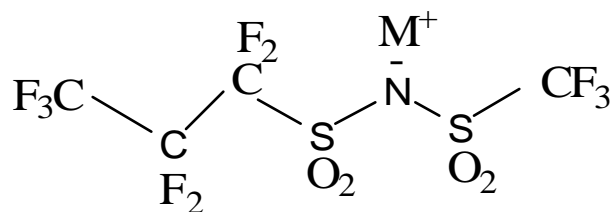
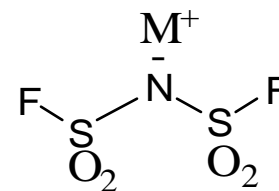
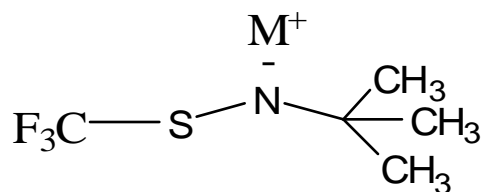
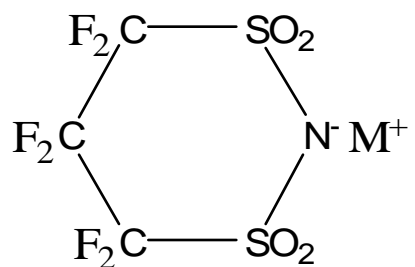
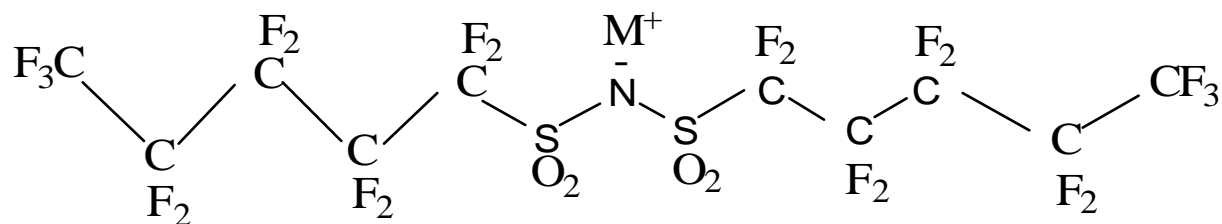


Detection of Cation Leaching of (a) [C4mim][PF6], (b) [C4mim][NTf2], and (c) [C4mim][BETI] via UV-Vis Spectra of Equilibrium Aqueous Phases

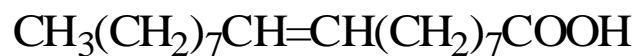
- The loss of the ILs was found to be strongly correlated to the conjugate anions. The more hydrophobic the anions are, the less are the losses of the ILs. The loss of C₄min-BETI is about 25 fold less than that of C₄min-PF₆.



Examples of Alkaline Metal Salts Can be Used to Produce a Variety of Ionic Liquids



Proton-Based Sacrificial Ion Exchangers

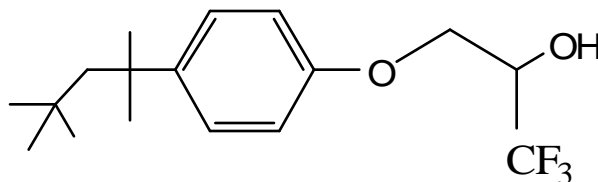


oleic acid

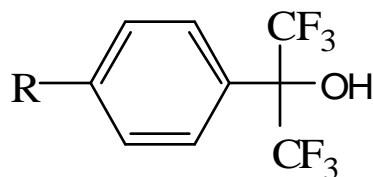
pKa: 4.8



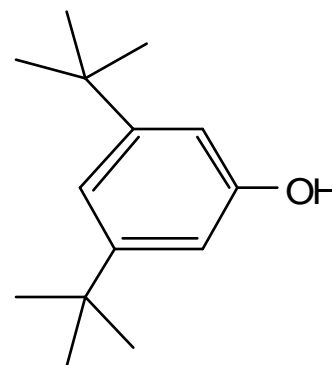
pKa: 20



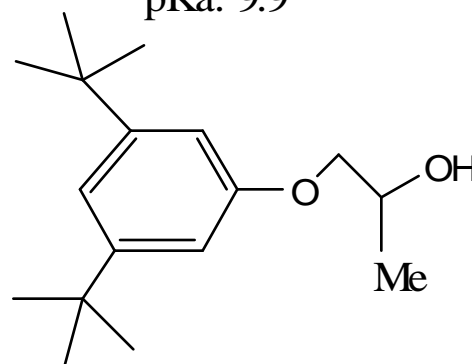
pKa: 12.5



pKa: 8.8




pKa: 9.9



pKa: 12.5

Moyer, B. A., etc. *Anal. Chem.* **2003**, 405

Effect of Carbon Chain Length of ILs and Synergistic Effect of Oleic Acid and Two Different Hydroxy Acids on Extraction Results of Rmim-Tf₂N Containing DCH18C6

Aq. Phase	Crown Ether	ILs containing Proton Exchanger	R in Rmim-Tf ₂ N			
			Ethyl, C2	Butyl, C4	Hexyl, C6	Octyl, C8
SrCl ₂	DCH18C6 0.02 M	NO	465.4	74.08	15.14	2.06
		 Oleic acid(1)	466.3	136.7	16.64	2.22
		Fluoro-(2)	465.9	64.3	15.85	1.82
		Di-tertbutylphenol (3)	419.0	58.7	12.48	1.71

ACKNOWLEDGEMENT

The work is supported by US Department of Energy, EMSP program project 81929.